

## AMENDMENTS TO THE CLAIMS

This Listing of Claims will replace all prior versions and listings of claims in this application.

Please cancel claim 14 without prejudice or disclaimer.

## Listing of Claims:

1. (Currently Amended) A process for preparing polytetrahydrofuran, polytetrahydrofuran copolymer, diester or monoester by polymerizing tetrahydrofuran in the presence of at least one telogen and/or comonomer and of an acidic heterogeneous catalyst not encompassing heteropolyacids and based on activated sheet silicates or mixed metal oxides in a fluidized bed,  
and wherein the reactor is operated in circulation and the ratio of circulation to feed is less than or equal to 200/l.
2. (Previously Presented) The process as claimed in claim 1, wherein the expansion factor of the catalyst bed is. less than or equal to 1.15.
3. (Previously Presented) The process as claimed in claim 1, wherein the expansion factor of the catalyst bed is from 1.01 to 4.
4. (Previously Presented) The process as claimed in claim 1, wherein the catalyst used comprises at least one oxide selected from the group consisting of SiO<sub>2</sub>, TiO<sub>2</sub> and ZrO<sub>2</sub>.
5. (Previously Presented) The process as claimed in claim 4, wherein the catalyst is based at least one material selected from the group consisting of on acid-activated montmorillonite, Al<sub>2</sub>O<sub>3</sub>/SiO<sub>2</sub>, ZrO<sub>2</sub>/SiO<sub>2</sub>, WO<sub>x</sub>/TiO<sub>2</sub>, and WO<sub>x</sub>/ZrO<sub>2</sub>.
6. (Previously Presented) The process as claimed in claim 1, wherein the-used has a pycnometric density of from 1.5 to 10 g/cm<sup>3</sup>.

7. (Previously Presented) The process as claimed in claim 1, wherein porosity of the catalyst is from 0.05 to 5 cm<sup>3</sup>/g.
8. (Previously Presented) The process as claimed in claim 1, wherein the individual catalyst particles have a volume of from 500 µm<sup>3</sup> to 5 cm<sup>3</sup>.
9. (Previously Presented) The process as claimed in claim 1, wherein the bed density of the catalyst is from 250 to 2500 g/l.
10. (Previously Presented) The process as claimed in claim 1, wherein the reactor is flowed through from bottom to top.
11. (Previously Presented) The process as claimed in claim 1, wherein the catalyst or portions of the catalyst volume are withdrawn from and/or fed to the polymerization reactor continuously, at regular intervals or batchwise, without the reactor being emptied and/or the polymerization reaction being interrupted for this purpose.
12. (Previously Presented) The process as claimed in claim 1, wherein tetrahydrofuran is polymerized in the presence of carboxylic anhydride to give polytetrahydrofuran or derivatives and copolymers thereof having molecular weights of from 250 to 10,000 dalton.
13. (Previously Presented) The process as claimed in claim 12, wherein the anhydride is acetic anhydride.
14. (Cancelled)
15. (Previously Presented) The process as claimed in claim 1, wherein the catalyst hourly space velocity is from 0.01 to 3.0 kg of THF/kg of catalyst per hour.
16. (Previously Presented) The process as claimed in claim 1, wherein the superficial velocity is from 0.1 to 200 m<sup>3</sup>/m<sup>2</sup> per hour.

17. (Previously Presented) The process as claimed in claim 6, wherein the catalyst used has a pycnometric density of from 2 to 7 g/cm<sup>3</sup>.

18. (Previously Presented) The process as claimed in claim 7, wherein the porosity of the catalyst is from 0.1 to 2 cm<sup>3</sup>/g.

19. (Previously Presented) The process as claimed in claim 18, wherein the porosity of the catalyst is from 0.2 to 1.5 cm<sup>3</sup>/g.